CLAIMS

1. A continuous process for forming extrudate of bioresorbable thermoplastic materials generally having constant cross-sections, comprising:

heating the material at a temperature higher than the melting point thereof and extruding the extrudate;

forming the extrudate;

controlling the formation of the extrudate to maintain a substantially constant shape by varying the speed of a motor driving the extruder;

cooling the extrudate after exiting the die by passing the extrudate through a cooling bath;

placing the extrudate under tension by passing the extrudate through a first puller adjacent the cooling bath and a second puller spaced from said first puller, said second puller running at a higher rate of speed than said first puller; and

heating the extrudate as it passes between said first and second pullers to a temperature above its glass transition temperature.

- 2. The process as set forth in claim 1 further including the step of passing the thermoplastic polymer extrudate through a die for forming said shape.
- 3. The process as set forth in claim 2 further including the step of controlling the extrusion rate of the extrudate from the extruder by using a metering pump and a feedback system to control the extruder motor speed.

- 4. The process as set forth in claim 3 wherein the metering pump controls the rate of extrudate flow into a die.
- 5. The process as set forth in claim 4 further including the step of measuring the cross-section of said extrudate after exiting said die.
- 6. The process as set forth in claim 1 wherein said material is heated to between about 125°C and 250°C prior to extrusion.
- 7. The process as set forth in claim 1 wherein said cooling bath contains water at a temperature between 10°C and 50°C .
- 8. The process as set forth in claim 1 wherein the polymer is selected from the group consisting of L-lactide, glycolide, D/L lactide, D-lactide and a combination thereof.
- 9. The process as set forth in claim 1 wherein the extrudate is heated between said first and second pullers to a temperature of between the glass transition temperature and the melting point.
- 10. The process as set forth in claim 1 wherein the extrudate is heated between said first and second pullers to a temperature of between 70°C and 200°C .

- 11. The process as set forth in claim 10 wherein the elongation is done in a heated water bath.
- 12. The process as set forth in claim 10 wherein the elongation is done in an air or inert gas oven.
- 13. The process as set forth in claim 1 wherein said material is annealed at a temperature of between about 70°C and 110°C while under said tension.
- 14. The process as set forth in claim 13 where the annealing is done for at least twenty minutes.
- 15. The process as set forth in claim 13 wherein said annealing is done in an air oven.
- 16. The process as set forth in claim 13 wherein said annealing takes place in a water bath.
- 17. The process as set forth in claim 1 wherein the extrusion is maintained in a single generally horizontal plane for the entire process.
- 18. The process as set forth in claim 1 wherein the extrusion is maintained in single generally horizontal and vertical planes for the entire process.

- 19. The process as set forth in claim 1 wherein said cooling of the extrudate after exiting the die cools the extrudate to below its glass transition temperature.
- 20. The process as set forth in claim 1 wherein the extrudate is heated between the first and second pullers to a temperature below the melting point of the polymer.
- 21. A continuous process for forming extrudate of bioresorbable thermoplastic materials generally having constant cross-sections, comprising:

heating the material at a temperature higher than the melting point thereof and extruding the extrudate;

forming the extrudate;

controlling the formation of the extrudate to maintain a substantially constant shape by varying the speed of a motor driving the extruder;

cooling the extrudate after exiting the die by passing the extrudate through a cooling bath;

placing the extrudate under tension by passing the extrudate through a first puller adjacent the cooling bath and a second puller spaced from said first puller, said second puller running at a higher rate of speed than said first puller;

heating the extrudate as it passes between said first and second pullers to a temperature above its glass transition temperature; and

releasing the tension on the extrudate after said second puller and prior to allowing the extrudate to cool to room temperature.